



Pillard Fuel Handling System

Acelerador de progreso



Pillard Fuel Handling System Pulverized Fuel General Overview



Pillard Fuel Handling System Heavy Oil General Overview





- Complete pre-mounted equipment from unloading to the burners :
 - > Unloading station
 - > Storage drawings
 - > Circulating pumps station
 - > High pressure pump station
 - > Heating sets
 - Control and safety valve trains



Pillard Fuel Handling System Example of Heavy Oil Equipment



High Pressure Pumping Set



Steam Heating Set



Flow control and shut off valve train

fives pillard



Pillard Fuel Handling System

Natural Gas General Overview

- Complete pre-mounted equipment from pressure reducing station to the burners :
 - Filtering station
 - Heating sets
 - > Pressure reducing station
 - > Flow measuring valve train
 - Control and safety valve trains



Pillard Fuel Handling System Example of Natural Gas Equipment



Filtering Station



Flow control and shut off valve train



Pressure Reducing Station

EXAMPLE OF GAS BURNERS





Gas gun on existing burner



Gas kiln burner



NATURAL GAS SYSTEM FOR BURNERS

Introduction to natural gas system design for cement plants

Date : March 8th, 2023 Prepared by H.Billig



VALVE TRAINS FOR BURNERS





VALVE TRAINS FOR BURNERS

BURNER MANAGEMENT SYSTEM

BMS AND LCP

Fives can supply the electrical cabinet for burner operation with all components for sequences and alarms, for gas flow control, visualization and supervision.

It can be installed in the electrical control room on close to the burner in a dedicated climatised shelter





GAS PRESSURE REDUCING STATION (BASIC)



2 FUNCTIONS:

- SAFETY : SHUT OFF VALVES

- PRESSURE REDUCING : PRESSURE REDUCER VALVE



PROCESS



GAS PRESSURE REDUCING STATION

GAS PRESSURE REDUCING STATION



WITH EXTRA FILTRATION AND HEATER



NECESSARY INFORMATION FOR A SUCESSFUL DESIGN GAS COMPOSITION

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Samp	ling Conditions	Mole %	NET Heat Value (81/07)	GAS Specific Gravity PURE
Comp	onent		0	0.9672
M _	Nitrogen	1.20	0	1.5195
·U2	Carbon Dioxide	0.971		1.1767
H ₇ S	Hydrogen Sulfide		580.8	0.5539
C,	Methane	81.233	909.4	1.0382
C,	Ethane	13.613	1618.9	1 5225
C1	Propane	2.646	2315.0	2 0068
IC.	i-Butane	0.162	3000.6	2.0000
nC.	n-Butane	0.154	3011.0	2.0008
C.	Neo-Pentane		3682.9	2.4911
10	i-Pentane	0.018	3699.1	2.4911
105	n.Qontane	0.004	3706.9	2.4911
nci	n-remains		4394.9	• 2.9754
C ₆	Hexanes		5091.0	3.4597
C,	Heptanes		5775.0	3.9440
C.8	Octanes		6493.2	4.4283
~9	Nonanes		3100.9	4.9126
Cie	Decanes +		/109.6	
Tota	1	100.00		
		Calcula	ted Whole Gas Properties	
	Dansity (Air=1 at	14,696 psia and 60*	F)-(Specific Gravity)	0.6648
Rea	Calculated Whole Gas Properties Relative Density (Alr=1 at 14.696 psia and 60*F) (Specific Gravity) Calculated Waight (0 / mol)			
INE	Relative Density (Alr=1 at 14.696 psia and 60°F) (Specific Gravity) ecular Weight (g / mol) ISITY LBS/SCF			0.0506
Cale	ulated Net Calorific Value ,	(B.T.U./CU.ft) (LHV)	1030.6894
Hve	trogen Sulfide ppmv			
Wa	ter content mg/l			

PROCESS

TECHNOLOGIES

What is important :

• Dry LHV,

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- Water contents,
- H₂S contents
- Nitrogen contents,
- Solid contents (particles)



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NECESSARY INFORMATION FOR A SUCESSFUL DESIGN TEMPERATURE AND PRESSURE AT THE GPRS INLET



PROCESS PARAMETERS					
SERVICE	DRYGAS	OUTLET DESIGN PRESSURE	100 Barg		
MAXIMUM OUTLET PRESSURE	60 Barg	INLET DESIGN PRESSURE	100 Barg		
FLOW RATE (SMNHR) (minimax)	2590 / 45500	DESIGN TEMPERATURE (minimax)	-10*0/60*0		
OPERATING PRESSURE (minimax)	20/50 barg				
OPERATING TEMPERATURE (minimax)	10*0/50*0				
INLET RATING	6°, 4500	7			
OUTLET RATING	8° , #500	7			
		1			

What is important:

- Inlet minimal temperature
- Inlet maximal pressure
- Design temperature
- Design pressure

PROCESS TECHNOLOGIES





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